305

Lecture #9 of 17

305

RECALL:

Geometry and... 306 ... uncompensated resistance models

(1) For working electrodes benefitting from convergent transport, worthwhile compensation is impossible unless a midget RE is positioned extremely close to WE.

(2) Uncompensated resistance declines dramatically as RE approaches WE; however, the angle of approach may be important.

(3) A large CE is effectively remote when its distance from the working electrode is at least 5 times the radius of WE.(4) When the CE is of a size comparable to that of WE, it is

effectively remote when the interelectrode distance is at least 10 times the radius of WE. (5) The resistance is effectively that of a cell in an infinitely

large vessel, if the vessel's radius exceeds that of the electrodes 5-fold.

(6) An electrode must be covered by at least 10 times its own radius of solution, before it is immersed in an effectively infinite volume.

Myland and Oldham, Anal. Chem., 2000, 72, 3972

306

307

Mass Transfer Processes

Chapters 1 and 4

308

Q: What's in this set of lectures?

A: B&F Chapters 1 & 4 main concepts:

- Section 1.4: Mass transfer and Semi-empirical treatment of electrochemical observations
- Chapter 4: Mass transfer

308

309

Looking forward... Section 1.4 and Chapter 4

- Mass transfer
- Diffusion
- Migration / Drift
- Convection
- Semi-empirical diffusive models
- Conductivity
- Transport (Transference) number
- Balance sheets
- Ohmic drop/loss

309





311

... mass transfer in electrochemistry is concerned with the movement of material = mass (even species as small as electrons) from one location (in solution) to another, and arises from spatial differences in electric potential, chemical potential, or from volume movement (of solution)...

... We need to understand mass transfer! ...

... but first, because it relates directly to mass transfer, I need to introduce the governing <u>equation for the continuity of mass</u>, which is even more stringent than the law of the conservation of mass!

311

... since the continuity of mass equation is "better than" the conservation of mass 312 law, and it is highly relevant to electrochemistry and in fact all science and engineering fields, we better know it...

... it is introduced to most undergraduate students studying chemical engineering, materials science, and physics, but only partially to chemists (first half) and mechanical engineers (second half)...

... anyway, here it is for species A along dimension x... Enjoy!

$$\frac{\partial c_{\rm A}}{\partial t} = \sum_{i} R_{{\rm A},i} - \frac{\partial N_{\rm A}}{\partial x}$$

https://en.wikipedia.org/wiki/Continuity_equation

312

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315

Mass transfer... which is similar to heat transfer... and momentum transfer 316

(1) Migration / Drift (no analogous term for heat, as heat is not charged) Flux (mol cm² s¹) of charged species due to an electric field (electric potential)... in general, stirring does not affect this as cations and anions move in opposite directions



http://wps.prenhall.com/wps/media/objects/3313/3392587/blb2003.html

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317

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 \dots FYI: even without intentional forced convection, unintentional forced convection (e.g. vibrations) influences an electrochemical experiment after ~30 seconds

318



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Mass transfer is driven (mostly) by gradients in electrochemical potential... 320

Mass transfer, for a charged species, seems like a current!

How is current density (J, A cm⁻²) related to flux (N, mol cm⁻² s⁻¹)?

- ... well, current density has units of A cm⁻² = C cm⁻² s⁻¹...
- ... and flux has units of mol cm⁻² s⁻¹...
- ... So what do we need to equate these? ...
- ... something with units of C mol⁻¹...
 - $J_x = z F N_x$... the Faraday constant... and z

The total current density, in one-dimension, due to all charged species is,

$$J_x = zFN_x = F\sum_i z_i \left(-\frac{D_{LX}c_i}{RT} \cdot \frac{d\bar{\mu}_i}{dx} + c_i v_x\right), \text{ and in 3D...}$$

$$J = zFN = F\sum_i z_i \left(-\frac{D_i c_i}{RT} \cdot \nabla \bar{\mu}_i + c_i v\right), \text{ where } \overline{\nu} \text{ is "del" (nabla)}$$

... where D_i is the diffusion coefficient of species i (in units of cm² s¹), c_i is the concentration (in units of mol cm³), β_i is the electrochemical potential (in units of J mol⁻¹), and v is the velocity of the solution (in units of cm s⁻¹)

320

Mass transfer is driven (mostly) by gradients in electrochemical potential... 321

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- ... and flux has units of mol cm⁻² s⁻¹... For derivation, see Bockris & Reddy, So what do we need to equate these?
- ... So what do we need to equate these? ... Modern EChem, Vol. 1, 2002, Section 4.4.15

... something with units of C mol⁻¹... $J_x = z F N_x$... the Faraday constant... and z

The total current density, in one-dimension, due to all charged species is, $L = \pi E N = E \sum_{i=1}^{n} \pi \left(\frac{|D_{i,x}c_i|}{2} \frac{d\mu_i}{d\mu_i} + \alpha \pi \right) \text{ and in 3D}$

$$\begin{split} J_x &= zFN_x = F\sum_i z_i \left(-\frac{\left| \sum_{l,x \in I} \right|}{RT}, \frac{d\mu_i}{dx} + c_i v_x \right), \text{ and in 3D...} \\ J &= zFN = F\sum_i z_i \left(-\frac{D_i c_i}{RT} \cdot \nabla \mu_i + c_i v \right), \text{ where } \nabla \text{ is "del" (nabla)} \end{split}$$

... where D_i is the diffusion coefficient of species *i* (in units of cm² s⁻¹), c_i is the concentration (in units of mol cm³), μ_i is the electrochemical potential (in units of J mol ⁻¹), and ν is the velocity of the solution (in units of cm s⁻¹)

321

Mass transfer is driven (mostly) by gradients in electrochemical potential... 322

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- ... and flux has units of mol cm⁻² s⁻¹...

... So what do we need to equate these? ...

... something with units of C mol⁻¹...

As we will see, besides the sign, this equals conductivity (a) divided by $z_{\ell-m}$, $J_x = z F N_x$... the Faraday constant... and z and thus in the absence of convection...

The total current density, in one-dimension, due to all charged species is,

$$\begin{split} J_x &= zFN_x = F\sum_i z_i \left(-\frac{D_{ix}c_i}{RT} \cdot \frac{d\overline{\mu}_i}{dx} + c_i v_x \right), \text{ and in 3D...} \\ J &= zFN = F\sum_i z_i \left(-\frac{D_{ic}}{RT} \cdot \overline{V}\overline{\mu}_i + c_i v \right), \text{ where } \overline{v} \text{ is "del" (nabla)} \end{split}$$

$$I_{ij} = \frac{\sigma_i}{\sigma_i} \frac{d\mu_i}{d\mu_j}$$
 how elegant and rather easy to memorize

... $J_{x,i} = \frac{1}{z_i F} \frac{1}{dx}$... how elegant... and rather easy to memorize ... where D_i is the diffusion coefficient of species *i* (in units of cm² s⁻¹), c_i is the

and ν is the velocity of the solution (in units of mol r^{-3}), $\bar{\mu}_i$ is the electrochemical potential (in units of J mol⁻¹), and ν is the velocity of the solution (in units of cm s⁻¹)

mass transport/transfer of molecules to the WE in an electrochemical cell 323 has three contributions: diffusion, migration/drift, and convection

the Nernst-Planck Equation:

$$J_i(x) = -D_i \frac{\partial C_i(x)}{\partial x} - \frac{z_i F}{RT} D_i C_i \frac{\partial \phi(x)}{\partial x} + C_i v(x)$$

the total **flux** of reactant *i* to a flat electrode (this is $N_i(x)$ in many textbooks - not ours! especially engineering ones; it has units of mol cm⁻² s⁻¹)



(1864–1941) (1858–1947) Nobel Prize (Chemistry, 1920) Nobel Prize (Physics, 1918) from Wiki

323

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$$J_{i}(x) = -\frac{D_{i} \frac{\partial C_{i}(x)}{\partial x}}{\int} -\frac{z_{i}F}{RT} D_{i}C_{i} \frac{\partial \phi(x)}{\partial x} + C_{i}v(x)$$

the diffusive flux of reactant *i* to a flat electrode where, again, D_i is the diffusion coefficient for species, i (D has units of cm² s⁻¹)

324

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$$J_{i}(x) = -D_{i} \frac{\partial C_{i}(x)}{\partial x} - \frac{z_{i}F}{RT} D_{i}C_{i} \frac{\partial \phi(x)}{\partial x} + C_{i}v(x)$$
B&F, 1.4.2

& 4.1.8

C_{i}v(x)

the flux due to migration/drift of reactant i where z_i is the charge on species i, and $\partial \phi / \partial x$ is the gradient in electric potential (which is equal to the negative of the electric field, E)

mass transport/transfer of molecules to the WE in an electrochemical cell 326 has three contributions: diffusion, migration/drift, and convection

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$$J_{i}(x) = -D_{i} \frac{\partial C_{i}(x)}{\partial x} - \frac{z_{i}F}{RT} D_{i}C_{i} \frac{\partial \phi(x)}{\partial x} + \frac{\overset{\text{B&F, 1.4.2}}{C_{i}v(x)}}{\overset{\text{B}, 1.4.2}{C_{i}v(x)}}$$

Т the flux due to convection of reactant *i* where v(x) is the velocity profile of the solution

326

mass transport/transfer of molecules to the WE in an electrochemical cell 327 has three contributions: diffusion, migration/drift, and convection

the Nernst-Planck Equation:

The vertex-Planck Equation:

$$J_{i}(x) = -D_{i} \frac{\partial C_{i}(x)}{\partial x} - \frac{z_{i}F}{RT} D_{i}C_{i} \frac{\partial \phi(x)}{\partial x} + C_{i}v(x)$$
B&F, 1.4.2

& 4.1.8

(4.1.8)

 \dots so, because we are adding up three contributions to the flux – which is proportional to the current (density) – if we drew a circuit to represent these terms, would these contributions be in series or in parallel?

... in parallel...
$$J_i(x) = J_1 + J_2 + J_3$$

327

mass transport/transfer of molecules to the WE in an electrochemical cell 328 has three contributions: diffusion, migration/drift, and convection

the Nernst-Planck Equation:

$$J_{i}(x) = -D_{i} \frac{\partial C_{i}(x)}{\partial x} - \frac{z_{i}F}{RT} D_{i}C_{i} \frac{\partial \phi(x)}{\partial x} + C_{i}v(x)$$
^{B&F, 1.4.2}
^{& 4.1.8}

... so, if $J_{migration/drift}$ is huge and $J_{diffusion}$ is small, what process dominates J?

J_{migration/drift}

... and now what if there was rapid stirring?

J_{convection}

mass transport/transfer of molecules to the WE in an electrochemical cell 329 has three contributions: *diffusion, migration/drift*, and *convection*

the Nernst-Planck Equation:

$$J_i(x) = -D_i \frac{\partial C_i(x)}{\partial x} - \frac{z_i F}{RT} D_i C_i \frac{\partial \phi(x)}{\partial x} + C_i v(x)$$

... again... but where did this equation for flux come from?

... who's comfortable with me just giving you this equation?

329

... first, recall our brief (more rigorous) "review" of thermodynamics... 330

Electrochemical potential of species *i* in phase β is an energy (J/mol),

$$\overline{\mu}_{i}^{\beta} = \left(\frac{\partial G}{\partial n_{i}^{\beta}}\right)_{T,p,n_{j\neq i}} = \frac{\mu_{i}^{\beta} + z_{i}F\phi^{\beta}}{\mu_{i}^{\beta} + z_{i}F\phi^{\beta}}, \text{ where }$$

G (Gibbs free energy (J)) n_i (amount of species *i* (mol)) $\mu_i = \mu_i^0 + RT \ln a_i$ (chemical potential (J/mol)) z_i (valency of species *i*) $F \approx 10^5$ (Faraday constant (C/mol) ϕ^{β} (Galvani/inner electric potential (V)) a_i (activity of species *i*)

For an uncharged species $\bar{\mu}_i^{\beta} = \mu_i^{\beta}$.

Parsons, Pure & Appl. Chem., 1973, 37, 501 IUPAC Gold (http://goldbook.iupac.org)

B&F, 1.4.2

330

... don't worry... there aren't too many steps...

331

From before, for one species the total flux in one-dimension is

 $N = -\frac{Dc}{RT} \cdot \frac{d\overline{\mu}}{dx} + c\nu, \text{ where again } D \text{ is diffusion coefficient (cm² s⁻¹), } c \text{ is }$ concentration (mol cm⁻³), $\overline{\mu}$ is the electrochemical potential (J mol⁻¹), ν is velocity (cm s⁻¹)

Recall that $\ \bar{\mu}_i^{eta} = \mu_i^{eta} + z_i F \phi^{eta}$ and so,

$$\begin{split} N &= -\frac{Dc}{RT} \cdot \frac{d(\mu^+ z F \phi)}{dx} + cv.. \text{ and recall that } \mu_i = \mu_i^{\ 0} + RT \ln a_i \text{ and so,} \\ N &= -\frac{Rc}{RT} \cdot \frac{d(\mu^0 + RT \ln a + z F \phi)}{dx} + cv. \end{split}$$

$$\int_{i}^{i} J_{i}(x) = -D_{i} \frac{\partial C_{i}(x)}{\partial x} - \frac{z_{i}F}{RT} D_{i}C_{i} \frac{\partial \phi(x)}{\partial x} + C_{i}\nu(x)$$

a...

... don't worry... there aren't too many steps...

From before, $\underline{\text{for one species}}$ the total flux $\underline{\text{in one-dimension}}$ is

$$\begin{split} N &= -\frac{Dc}{RT} \cdot \frac{d\bar{\mu}}{dx} + c \upsilon, \, \text{where again D is diffusion coefficient (cm² s³), c is}\\ \text{concentration (mol cm³), $\bar{\mu}$ is the electrochemical potential (J mol²), v is velocity (cm s³)}\\ \text{Recall that $$\bar{\mu}_{\rm f}^{\beta} = \mu_{\rm f}^{\beta} + z_{\rm f} F \phi^{\beta}$ and so,} \end{split}$$

$$N = -\frac{Dc}{RT} \cdot \frac{d(\mu + zF\phi)}{dx} + cv... \text{ and recall that } \mu_i = \mu_i^0 + RT \ln a_i \text{ and so,}$$

$$N = -\frac{Dc}{RT} \cdot \frac{d(\nu^0 + RT \ln a + zF\phi)}{dx} + cv... \text{ and assuming } \sigma \approx c,$$

$$N = -Dc \cdot \frac{d(\ln c)}{dx} - \frac{zFD}{RT} c \cdot \frac{d\phi}{dx} + cv... \text{ and finally...}$$

$$J_i(x) = -\frac{D_i}{D_i} \frac{\partial C_i(x)}{\partial x} - \frac{Z_i F}{RT} \frac{D_i}{D_i} C_i \frac{\partial \phi(x)}{\partial x} + C_i v(x)$$

332

Some very important background "first" ... okay, second!

333

Diffusion coefficient (*D***, cm² s⁻¹)** – "proportionality constant relating the flux of [the] amount of [an entity to its] concentration gradient..." (IUPAC Gold Book)

Fick's first law of steady-state Diffusion: $N_z = -D_z \frac{dc}{dz}$ in 1D (His second law is for non-steady-state conditions, where time is another independent variable.)



333

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334

Diffusion coefficient (D, **cm**² **s**⁻¹) – "proportionality constant relating the flux of [the] amount of [an entity to its] concentration gradient..." (IUPAC Gold Book)

Fick's first law of steady-state Diffusion: $N_z = -D_z \frac{dc}{dz}$ in 1D D also exhibits Arrhenius behavior: $D = D_0 e^{-\frac{E_\alpha}{RT}}$ where D_0 is the maximum D (at infinite T) where D_0 is the maximum D (at infinite T) G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0 G < 0G < 0 Steady-state? Initial states equilibrate using ICE, ICE Baby!

I	0.150 M	0.000 M	0.000 M
с	-x M	+x M	+x M
E	0.150 - x M	× M	×М



335

A <mark>≓</mark> B + C

Vanilla Ice wants to know, "As the initial state progresses, what happens if you keep supplying A and pulling B and C away?" ...

335

... Le Chatelier's Principle keeps the reaction going ...

336

 \rightarrow A \rightleftharpoons B + C \rightarrow

... but for how long? ...

$$M_1 \rightarrow A \rightleftharpoons B + C \rightarrow M_2$$

... as long as the rate of supply in and the rate of exit out are constant... ... and in electrochemical systems, as long as a constant potential bias is applied!

In an ideal world, i.e. under certain rare conditions,

 $\frac{\partial c_A}{\partial t} = \frac{\partial c_B}{\partial t} = \frac{\partial c_C}{\partial t} = 0$, and the system is in a <u>steady-state</u> where there is a net flux of species (generation of A, from the left, and loss of B & C, to the right) but the species concentrations in the cell do not change with time

336

Who cares? ...

337

... when the current is at a steady-state, *the current is constant*, and there is no new capacitive charging!

$$M_1 \rightarrow A \rightleftharpoons B + C \rightarrow M_2$$

... for steady-state current, KCL applies... no, not KCI... but KCL!

Kirchhoff's Current Law (KCL)

$$\sum_{k=1}^{n} I_k = 0$$



http://en.wikipedia.org/wiki/Kirchhoff%27s_circuit_laws

But KCL applies to the *entire circuit*, including in the potentiostat! 338 (when current flows, i.e. due motion of charges, it is the same everywhere in the circuit)



... hey, what are those minus signs at the bottom? ...

Migrating/Drifting lons!

... we'll get to this shortly

338

Back to the first flux term... Diffusion...

339

Diffusion coefficient (*D***, cm² s⁻¹)** – "proportionality constant relating the flux of [the] amount of [an entity to its] concentration gradient..." (IUPAC Gold Book)

Fick's first law of <u>steady-state</u> Diffusion: $N_z = -D_z \frac{dc}{dz}$ in 1D



Do the units of D make senser N_{z} (mol cm² s⁻¹, as xy) = D_{z} · (mol cm⁻³) cm⁻¹, as xyz z) (mol cm² s⁻¹, as xy) = D_{z} · (mol cm⁻⁴, as xyzz) Therefore, D_{z} is has units of cm² s⁻¹... but as zz...

Huh? zz? z2? What?... That was unexpected!... Is it right?...

Adolf Eugen Fick (1829–1901) from Wiki

Physician & Physiologist

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